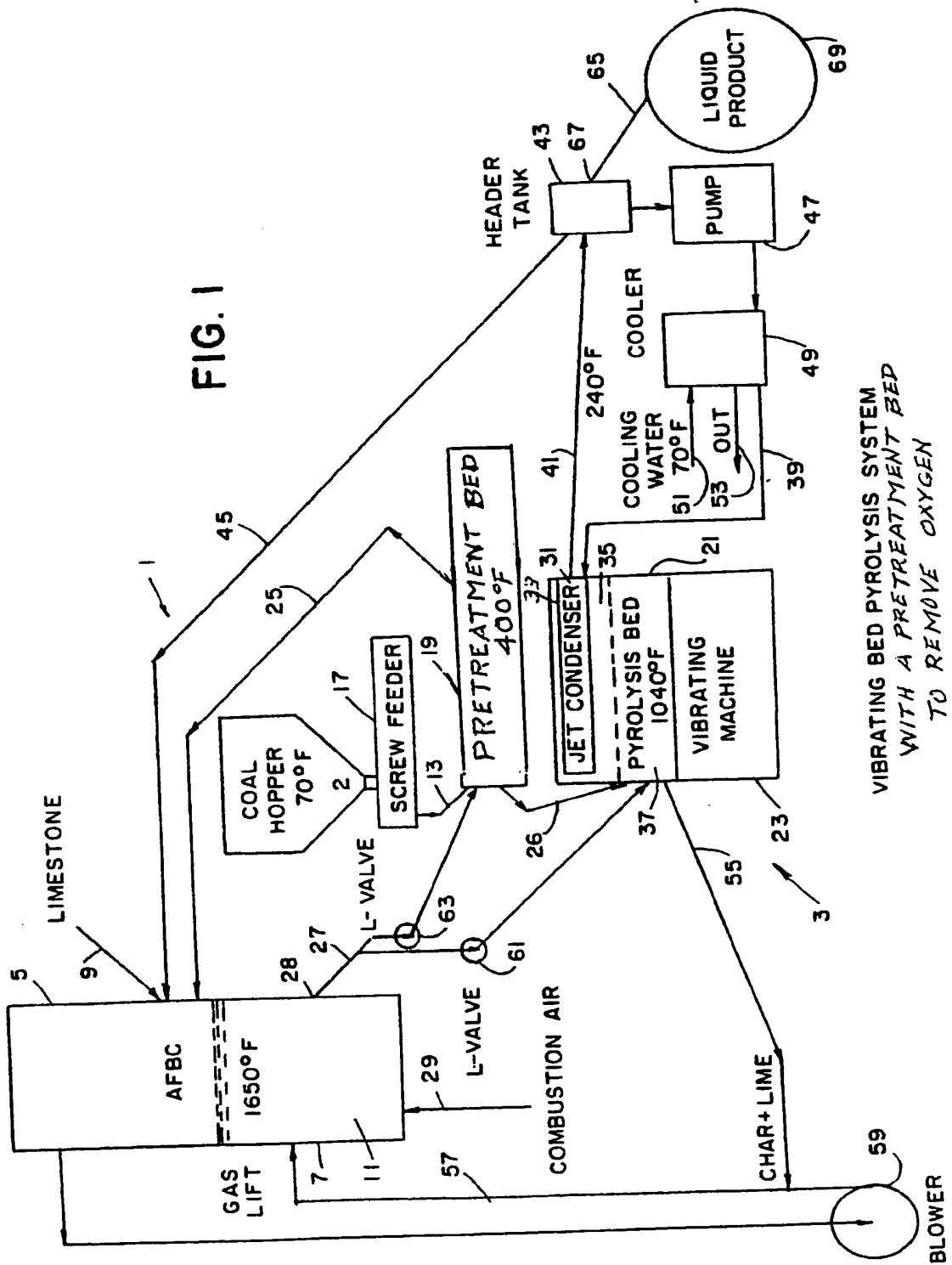


—  
EIG.  
—



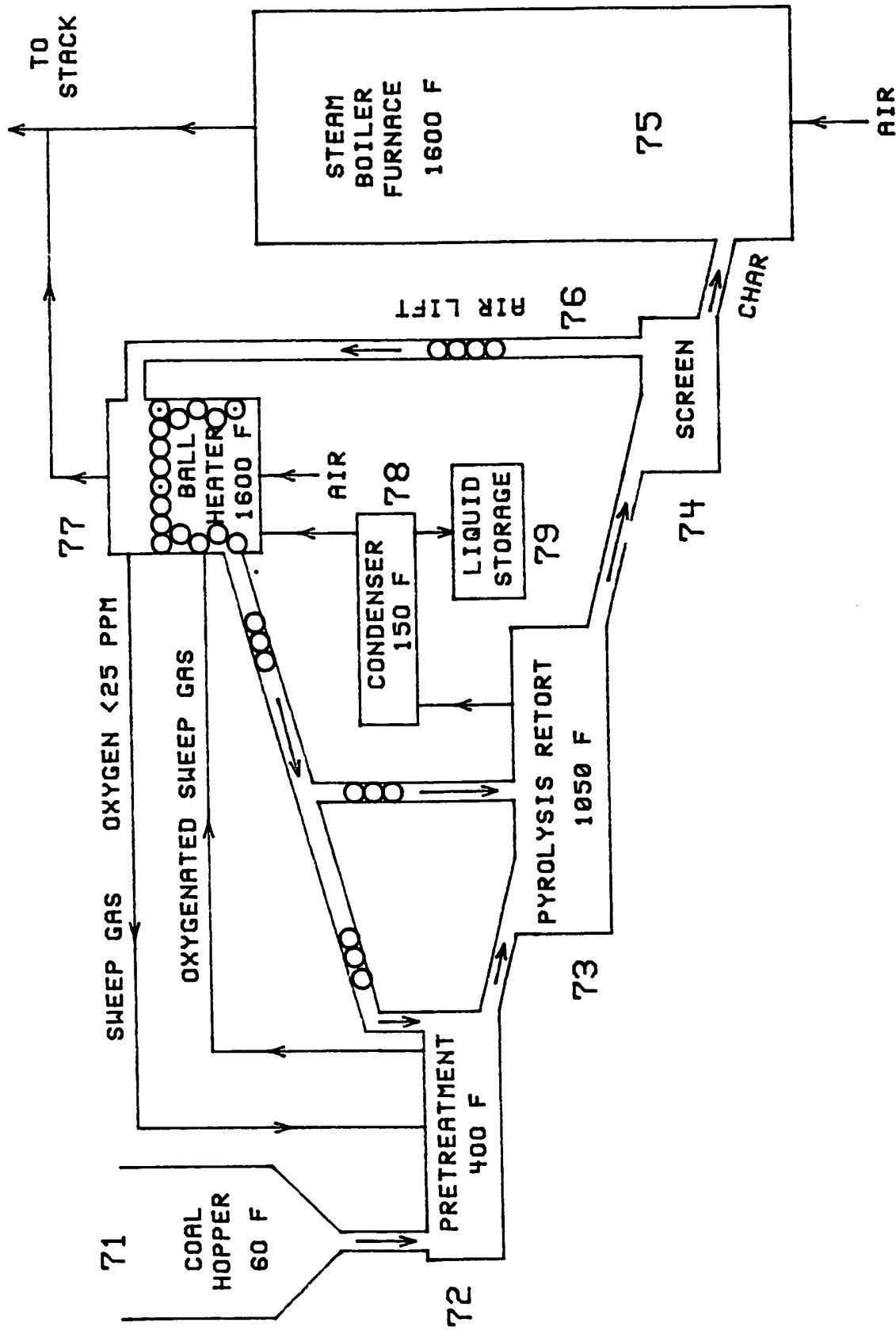
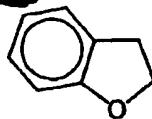


FIG. 2 COAL PRETREATMENT SYSTEM INCORPORATED IN A PYROLYSIS PROCESS UTILIZING CERAMIC BALLS FOR TRANSPORTING HEAT BETWEEN COMPONENTS

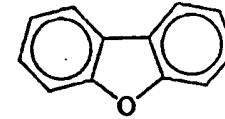
The most common form of heterocyclic oxygen is in furan ring systems:



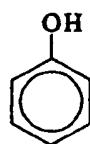
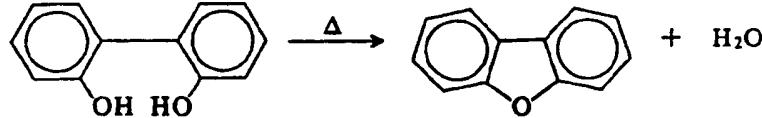
Furan



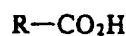
Benzofuran



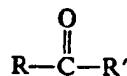
Dibenzofuran



Phenol



Carboxylic acid



Carbonyl



Aniline



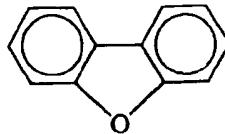
Pyridine



Quinoline



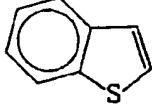
Ether



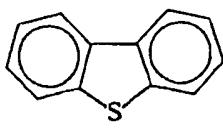
Heterocyclic oxygen



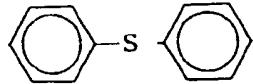
Thiophene



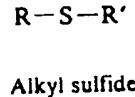
2,3-Benzothiophene



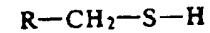
Dibenzothiophene



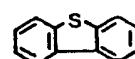
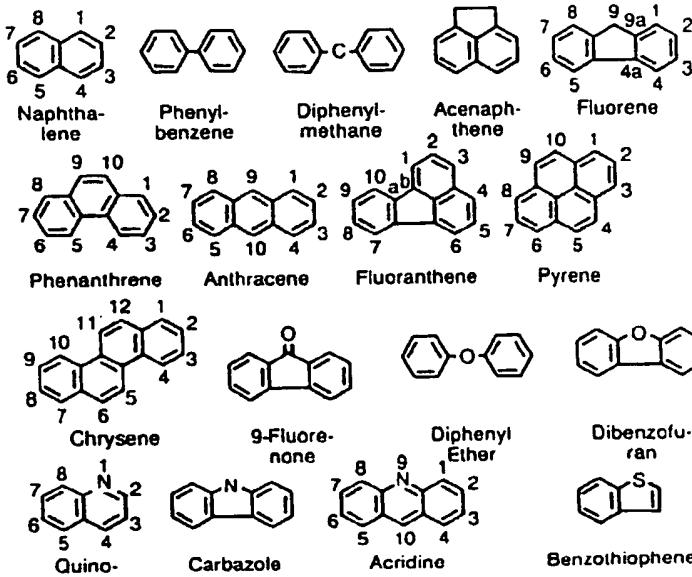
Diphenyl sulfide



Alkyl sulfide



Thiol



Dibenzothiophene

FIG. 3A Structure of selected model compounds.

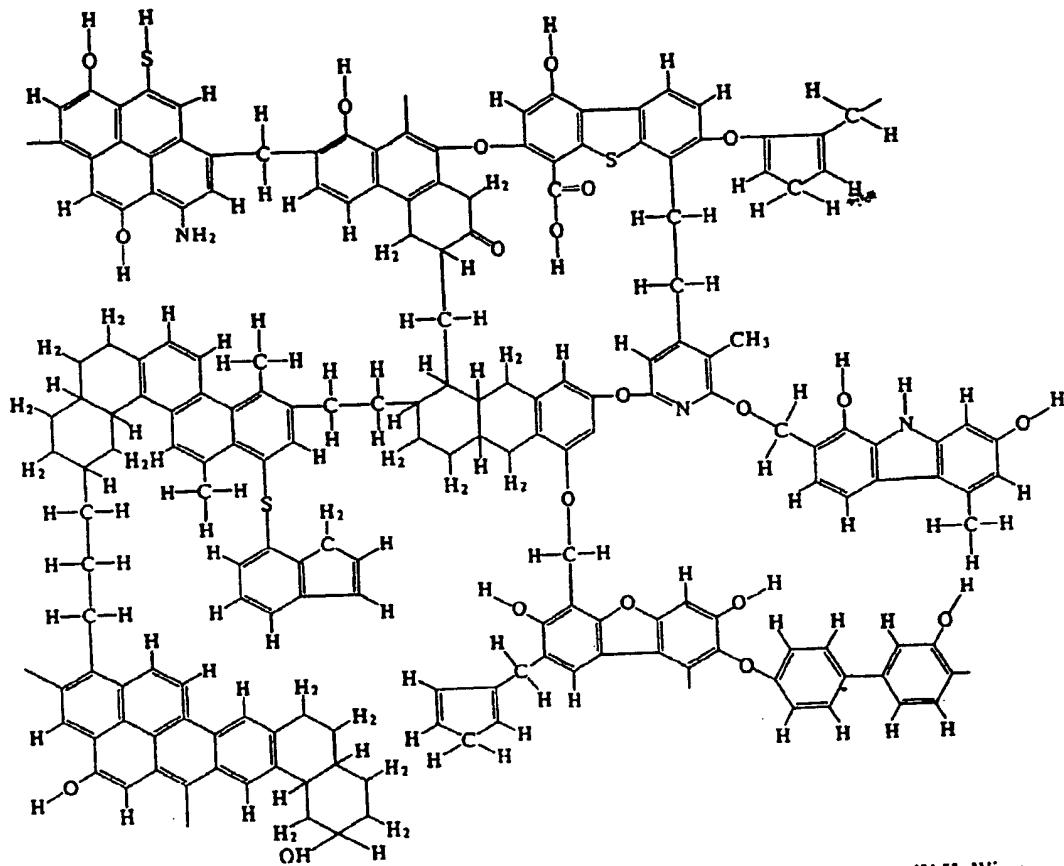


FIG. 3B Wiser model for bituminous coal. (Source: Reprinted with permission from W.H. Wiser, "Schematic Representation of Structural Groups and Connecting Bridges in Bituminous Coal," 1978.)

FIG. 4

GLASS SYSTEM PYROLYSIS TESTS

TEST NO. 10 - DEGASSING

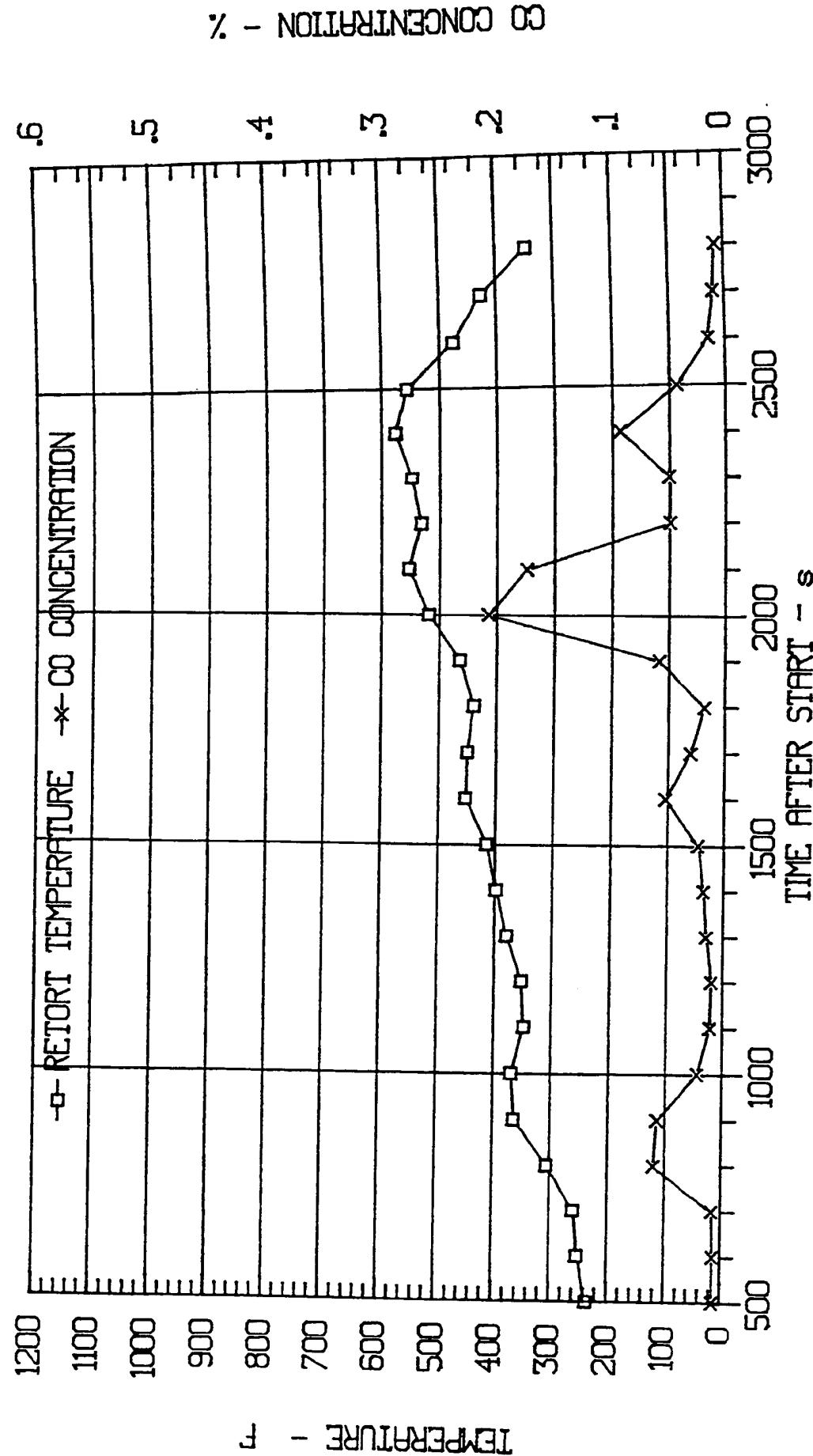
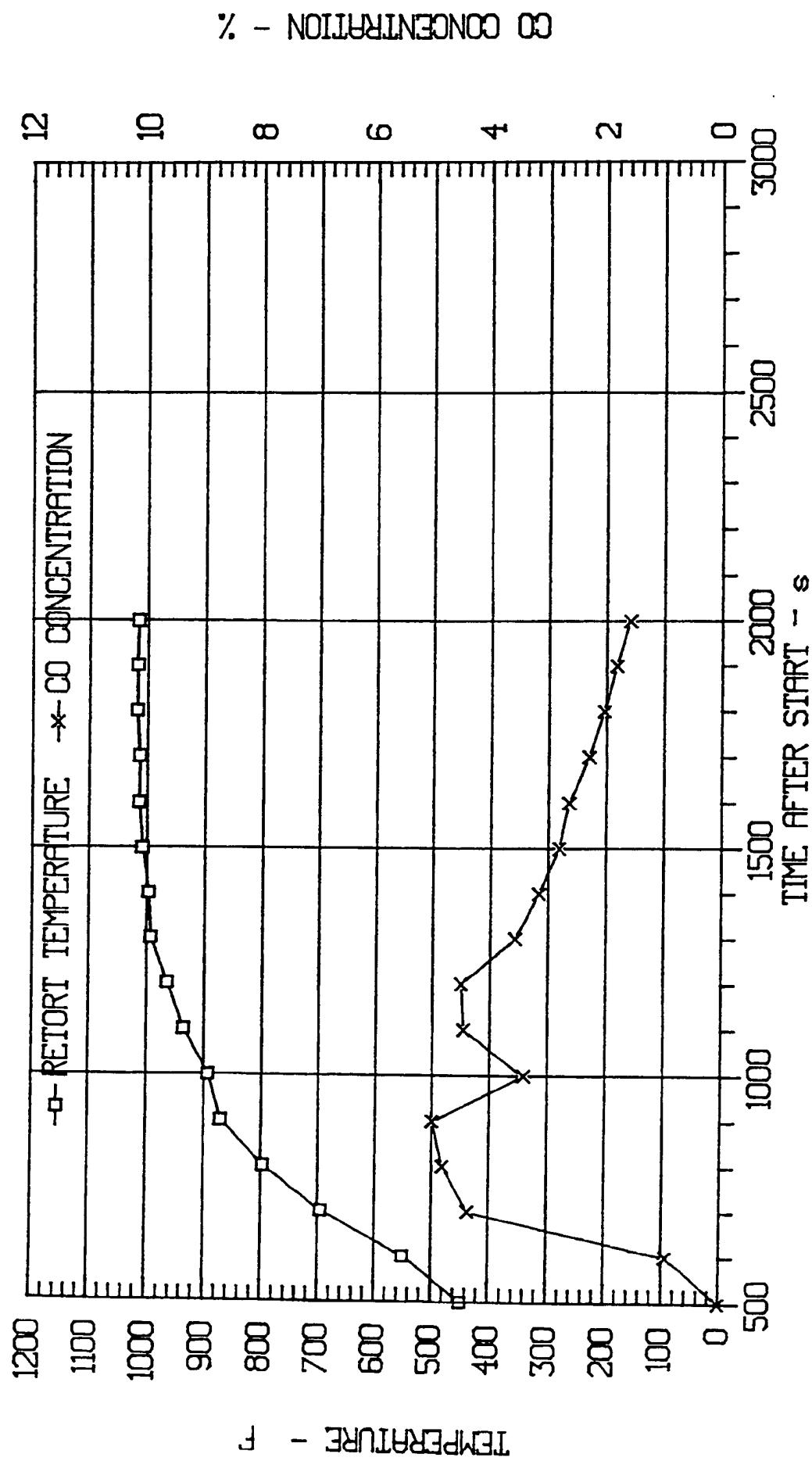


FIG. 5

GLASS SYSTEM PYROLYSIS TESTS

TEST NO. 10 - PYROLYSIS



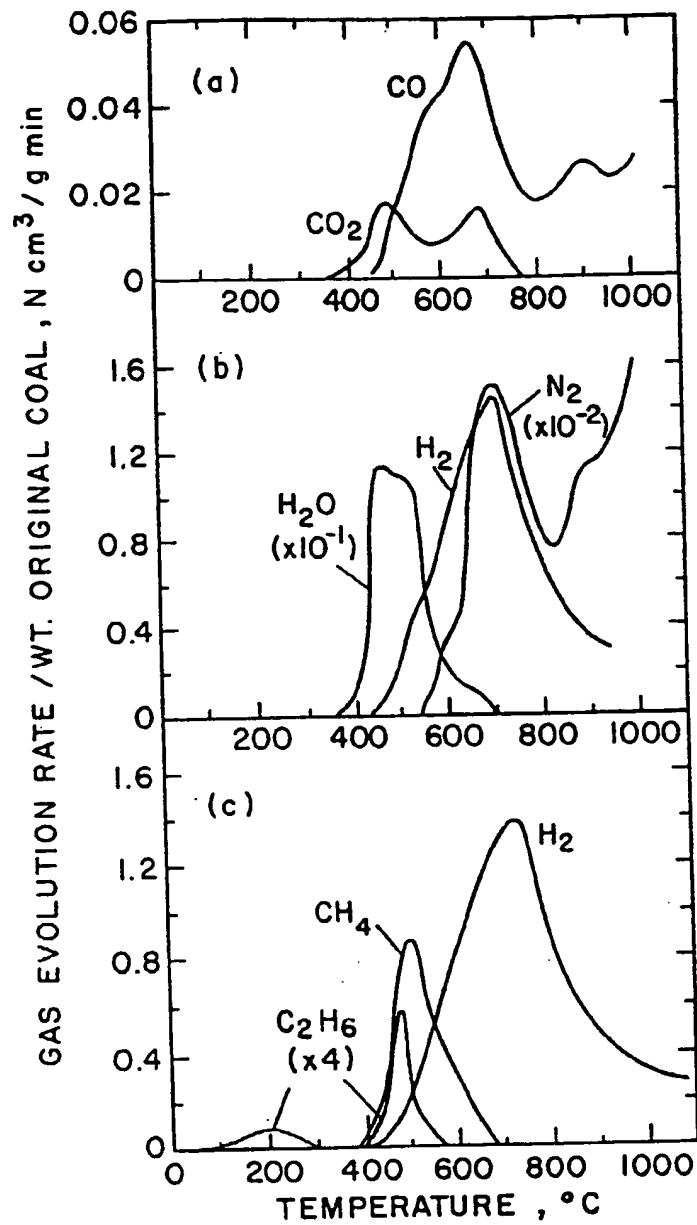


FIG. 6 Variation of Gaseous Species Evolution with Temperature during Coal Pyrolysis at Constant Heating Rate [(a) and (b), data of Klein (1971); (c), data of Gustav coal, VM = 29 wt. % (MAF): heating rate =  $1^{\circ}\text{C}/\text{min}$ . (c), data of Jüntgen and Van Heek (1968): VM = 19.1 wt. %; heating rate =  $2^{\circ}\text{C}/\text{min}$ ].

FIG. 7 Oxygen concentration in the off-gas and pretreatment bed temperature as functions of time from initiation of nitrogen purge.

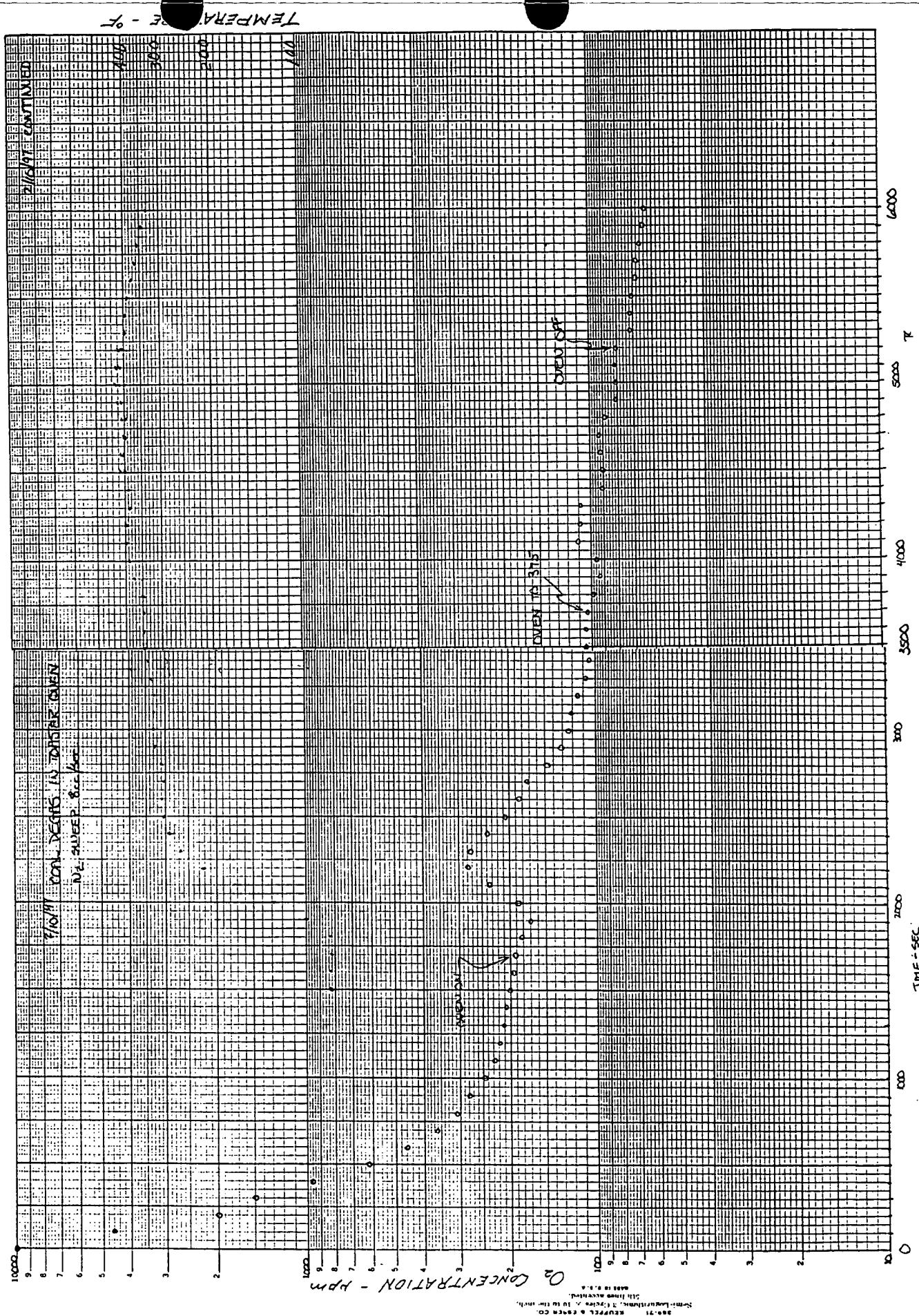


FIG. 8 Mass spectograph for pyrolysis product liquid after  
pretreatment at 450°F to remove oxygen. (Courtesy, NREL)  
01025637: Scan Avg 8-13 (0.99 - 1.62 min) - Back

